

AMENDMENTS TO THE CLAIMS

1. (Previously presented) A process for isomerizing cis-2-pentenitrile to trans-3-pentenitrile in the presence of aluminum oxide as a catalyst, wherein the aluminum oxide has a BET surface area of at least $50 \text{ m}^2/\text{g}$ and the reaction is carried out at a temperature in the range of from 50°C to 250°C .
2. (Original) The process according to claim 1, wherein the aluminum oxide has a BET surface area of at least $70 \text{ m}^2/\text{g}$.
3. (Original) The process according to claim 1, wherein the aluminum oxide has a BET surface area of at most $400 \text{ m}^2/\text{g}$.
4. (Previously presented) The process according to claim 1, wherein the isomerization is carried out in the liquid phase.
5. (Previously presented) The process according to claim 1, wherein the reaction is carried out at a temperature of at least 120°C and at most 200°C .
6. (Previously presented) The process according to claim 2, wherein the isomerization is carried out in the liquid phase and the aluminum oxide has a BET surface area of at most $400 \text{ m}^2/\text{g}$.
7. (Previously presented) The process according to claim 6, wherein the reaction is carried out at a temperature of at least 120°C and at most 200°C .
8. (Previously presented) The process according to claim 1, wherein the aluminum oxide has a BET surface area of at least $100 \text{ m}^2/\text{g}$.
9. (Previously presented) The process according to claim 1, wherein the aluminum oxide has a BET surface area of at most $300 \text{ m}^2/\text{g}$.
10. (Previously presented) The process according to claim 7, wherein the aluminum oxide has a BET surface area of at least $100 \text{ m}^2/\text{g}$ and at most $300 \text{ m}^2/\text{g}$.

11. (New) The process according to claim 1, wherein the aluminum oxide has a BET surface area of at least $50 \text{ m}^2/\text{g}$ and at most $400 \text{ m}^2/\text{g}$.
12. (New) The process according to claim 4, wherein the aluminum oxide has a BET surface area of at least $50 \text{ m}^2/\text{g}$ and at most $400 \text{ m}^2/\text{g}$.